

Scaling and Estimation

Physics 281

Lecture 1 - Buckingham Pi Theorem
⇒ Systematics of Dimensional Analysis

* - context: drag

→ Here consider systematics of dimensional analysis; scaling arguments.

→ Why scaling?

- real problems - nonlinear
- ↓
- many degrees freedom

- need estimation, guided to computation
N.B. {computers} are poor at asymptotics
but asymptotic fundamentals

→ Common issues:
describes

- self-similarity → ^{concept in} problems where phenomena "look the same", over broad range of scales

e.g. { boat wave
turbulence

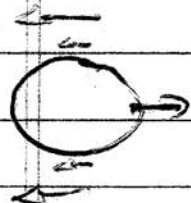
⇒ scaling relations constitute "the answer"

→ emergent scale \Rightarrow i.e. nonlinear dynamics defines "new scale"; e.g. Rhines scale, i.e. usually $\ln \sim \ln \ln$ behavior.

→ new physics ... (it happens!)

→ boundary layers \Rightarrow transition between scaling regimes

← different



no slip b.c.

$$V_T|_{\text{surf}} = 0$$



\sim potential flow far from body

\sim boundary layer near body, viscosity important

\Rightarrow different scalings, which must be matched.

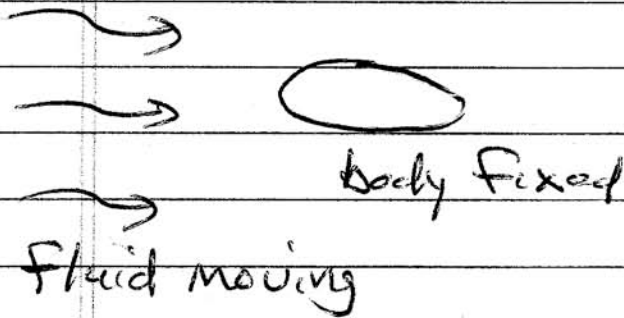
\Rightarrow Basic Question:

→ How Formulate Systematics of Dimensional Analysis? Limitations?

→ When might it fail?

→ What, really, is drag?

Consider frame where:



Drag \equiv rate of removal of momentum
from moving fluid by immersed
body

'Removal' \rightarrow transmission in boundary,
surface layer
 \rightarrow no-slip condition / viscosity

leaves wake \Rightarrow water acts to fill
in dead region

$$\Delta p / \Delta t \sim F_d \sim \rho A V^2$$

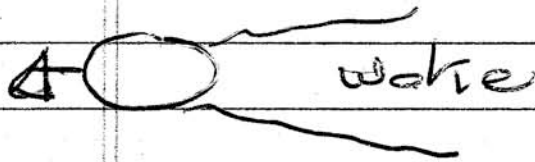
$$\sim C_D \rho A V^2$$

C_D captures additional physics.

Why additional physics? \rightarrow see 3q

(Why not formula valid?)

\Rightarrow - drag \Leftrightarrow wake \rightarrow



ahead - behind asymmetry



wake \rightarrow irreversibility
see 4q, contrast

- wake is consequence of no-slip b.c.

due. $v_T(r) = 0$

- in potential flow, $\nabla^2 \phi = 0$
 $\underline{u} = \nabla \phi$

v_T can be large \Leftrightarrow no wake

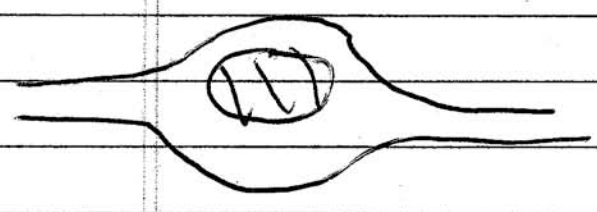


$$\Delta v_1 = \Delta v_2$$

Δv_{trans} deflection
same upstream
downstream!

ideal fluid

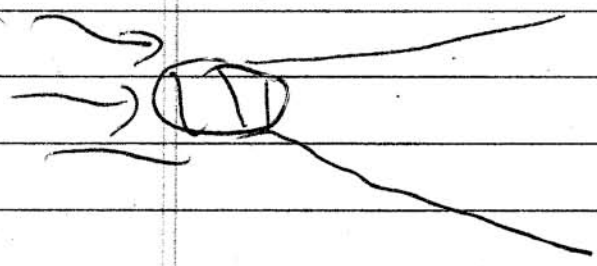
Euler eqn.
reversible



← vs → reversible

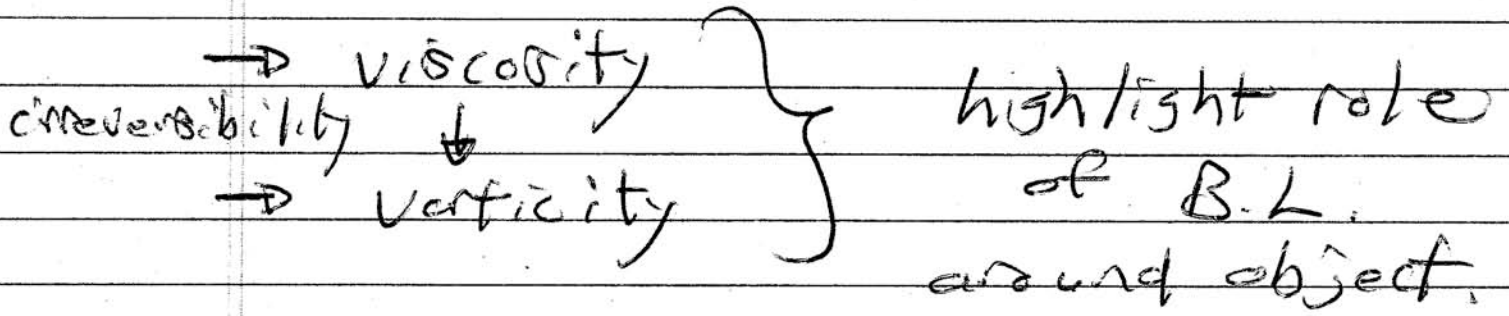
viscous fluid

N-S Eqn.
irreversible



← vs → clearly different

- wake, and thus drag, are due to



A.k.a highlights role of boundary layers \leftrightarrow drag can be independent of Re , but viscosity needed to satisfy b.c.

- additional physics \rightarrow model

Model \rightarrow Navier-Stokes Equation $\nabla \cdot \underline{v} = 0$
kinematic viscosity

$$\rho \left(\frac{\partial \underline{v}}{\partial t} + \underbrace{\underline{v} \cdot \nabla \underline{v}}_{\text{advection nonlinear}} - \underbrace{\nu \nabla^2 \underline{v}}_{\text{linear, 2nd order}} \right) = -\nabla p$$

$[\nu = 0 \text{ is singular}]$

Compressible NS Eqn:

$$\rho \frac{d\mathbf{u}}{dt} = -\nabla p + \rho \nu \nabla^2 \mathbf{u} + (\eta + \mu) \nabla(\nabla \cdot \mathbf{u})$$

$$\sigma = \text{const}, \quad ds = 0$$

$$\therefore \frac{dP}{\rho} = v dp - T ds = dw$$

enthalpy

mostly

- $\nabla \cdot \underline{v} = 0 \rightarrow$ determined pressure

- $\nabla \cdot \underline{v} \neq 0 \rightarrow$ need eqn. state.

dimensionless

Key Parameters:

$$\textcircled{1} / \textcircled{2} \equiv \text{Reynolds \#}$$

$$\approx \text{Re} \sim vL/\nu$$

Models (i.e. eqns) are useful to identify dim-less parameters

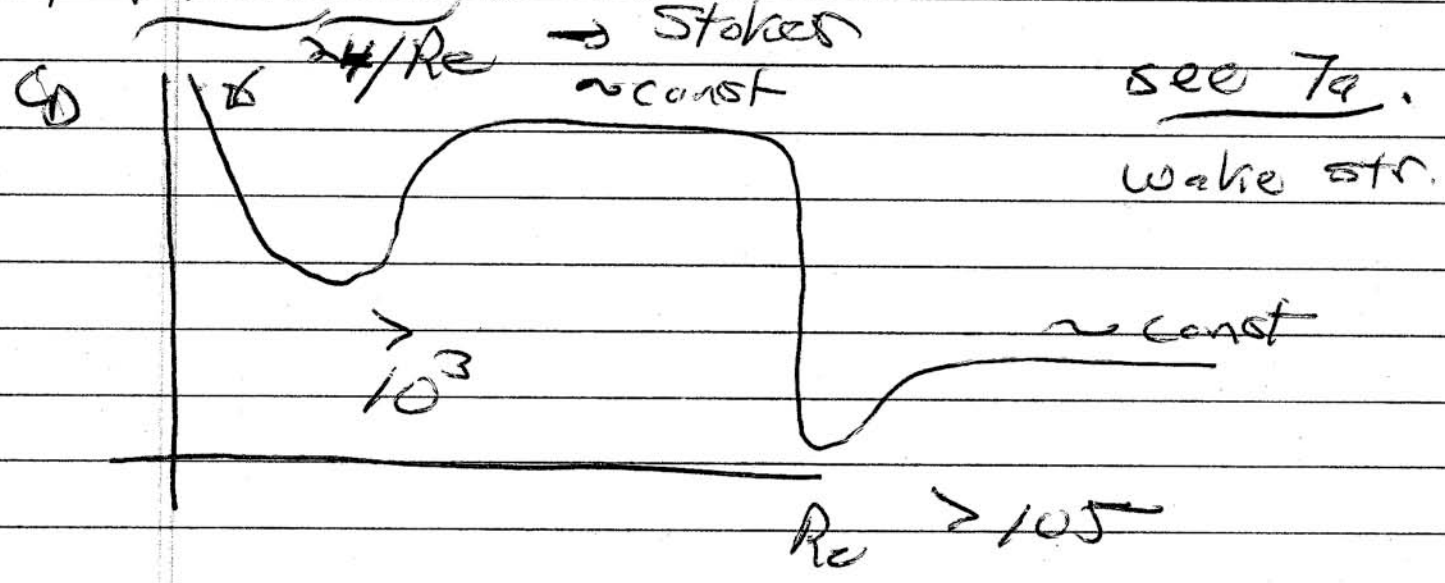
expresses ratio of nonlinear, inertial term to linear, diffusive term.

$\text{Re} < 1 \rightarrow$ viscous flow - Stokes

$\text{Re} > 1 \rightarrow$ laminar flow - Blasius

$\text{Re} > 10^5 - 10^6 \rightarrow$ turbulent flow.

→ the facts:



See especially: → basic trends

→ small Re regime → Stokesian regime

$C_D \sim 1/Re$

$\boxed{F_d \sim v}$

ie. $\frac{\partial v}{\partial t} + v \frac{\partial v}{\partial x} - \nu \frac{\partial^2 v}{\partial x^2} = -\frac{\partial p}{\partial x}$
 $\frac{\nu}{Re \ell} = -\frac{\partial p}{\rho}$

→ large Re → turbulent

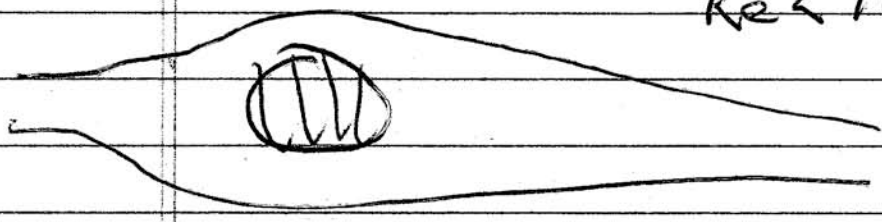
$C_D \sim Re^{\alpha}$

→ notable, why?

How recover scalings?

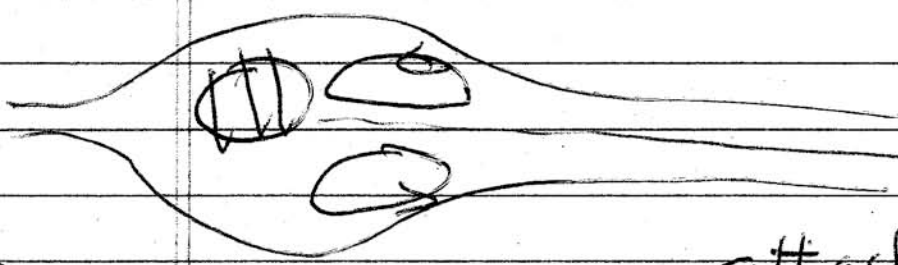
Wake structure: (cyl.)

$Re < 10$



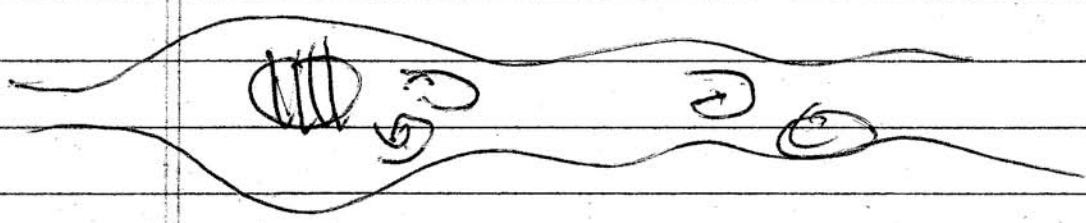
creeping flow

$10 < Re < 40$



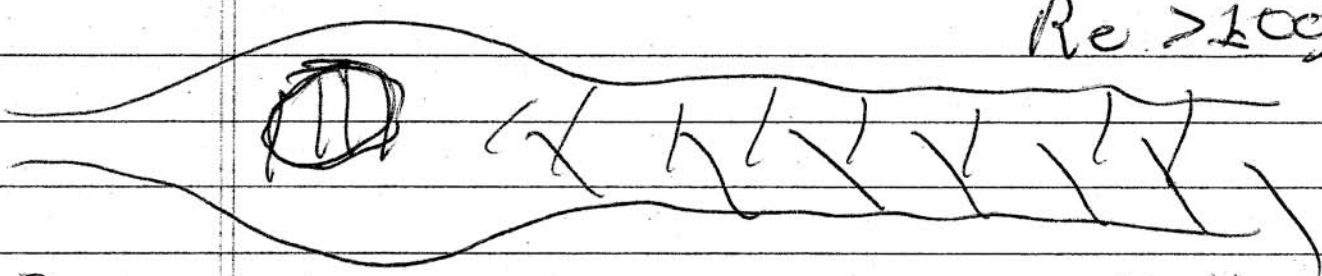
attached vortices

$40 < Re < 200,000$



vortex trail

$Re > 200,000$



turbulent wake

⇒ Buckingham's Pi Theorem

- e.x. first

- how do dimensional analysis systematically?

① - identify physically relevant variables
e.g. n of these

→ required answer should depend on relevant variables, and be listed among.

so, for drag on sphere:

steady

temp.

$v \sim v_{th} \ln \mu_{exp}$
↑
lower in water

$R \rightarrow$ length L

$V \rightarrow$ velocity L/T

$\nu \rightarrow$ viscosity (diffusion) L^2/T

{ water $\rightarrow 10^{-6} m^2/sec$
air $\rightarrow 10^{-5} m^2/sec$

$\rho \rightarrow$ fluid density M/L^3

$F_d \rightarrow$ drag force $F_d \sim ML^2/T^2$

② Count indep. dimensions

$\Rightarrow M, L, T$

so $n = 5$ quantities

$r = 3$ indep. dim.

\Rightarrow

③ $n - r = 2$ dimensionless ratios possible

1 involves F_d .

\Rightarrow Pi theorem

$n \rightarrow$ indep. quantities

$r \rightarrow$ indep. dimensions

$\therefore n - r$ dimensionless ratios s/t

$$\left[\begin{array}{l} \pi_i = F(\pi_1, \pi_2, \dots, \pi_{i-1}, \pi_{i+1}, \dots, \pi_n) \\ \text{i.e. can express dimensionless ratios} \\ \text{in terms each other} \end{array} \right.$$

Practical Matters

→ one π involved answer

→ other π 's involve relevant dim-less parameters, in model.

⚡
n.b. here = model → useful.

→ use insight # values (i.e. experiment) to eliminate some π variables

i.e. $\ll 1$, or $\gg 1$

back to sphere example:

→ 2 π variables.

where $\pi_1 = F(\pi_2)$

i.e. $\pi_1 = F_d / \rho_0 R^2 V^2 \rightarrow$ involves order

$\pi_2 = Re = VR/\nu \rightarrow$ suggested as natural dimensionless ratio from model

and π_c theorem \Rightarrow

$\pi_1 = \pi_1(\pi_2) = F(\pi_2)$

\Rightarrow $F_d = F(Re) \rho_0 R^2 V^2$ } π theorem result for drag.

- basic result
- plausible that drag depends on Re
- not a unique answer

Now, key step:

- explore asymptotic behaviour, i.e.

$Re \ll 1, Re \gg 1 ?$

→ $Re \ll 1$

- have $F_d \sim \rho_0 R^3 V^2 f(Re)$

- $Re \ll 1 \rightarrow$ expect $F_d \sim v$

i.e. proportional to viscosity

so

$f(Re) \sim 1/Re$, for $Re \ll 1$.

$$F_d \sim \rho_0 R^3 V^2 \frac{v}{RV} \sim [\rho R V] v$$

$$F_d \sim [\eta R] v \sim \eta R v$$

- corresponds to Stokesian flow drag

- general result:

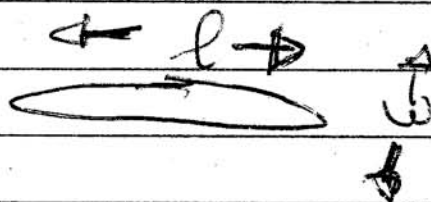
$$EOM: \quad -\nu \nabla^2 \underline{u} = -\frac{\nabla p}{\rho}$$

longest dim.

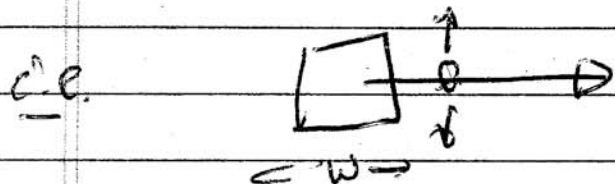


$$F_d \sim 6\pi\eta l v$$

$$\eta = \rho \nu$$



— Consider flat plate moving head on:


 $Re \ll 1$

Show Stokes scaling applies!

$$F_d \sim PA \sim \rho l w$$

for P

$$\nu \nabla^2 v = - \frac{\nabla p}{\rho}$$

what is the scale? \rightarrow smaller will dominate gradients

\Rightarrow

$$\frac{\rho}{\rho w} \sim \frac{\nu}{w^2} v$$

so

$$P \sim \frac{\rho r V}{w}$$

$$F_d \sim PA \sim \frac{\rho r V}{w} (w l)$$

$$\sim [\rho r l] V \quad \checkmark$$

Show for edge-on incidence - HW!

Now, for $Re \gg 1$, expect,

~~but~~ $F_d \sim V^2$

but

$$F_d \sim \rho V^2 R^2 f(Re)$$

$$\sim \rho V^2 R^2 Re^0 \rightarrow \rho V^2 R^2$$

so $Re \rightarrow \infty$

$$F_d \sim \rho V^2 R^2$$

Note:

- $f(Re) \sim Re^\alpha$ unsure about small
 $\alpha \ll 1$ corrections to α
 is possible

- amazing that $F_d \sim Re^{(6)}$ at
 large Re !

No ν dependence!

yet drag requires viscosity!

Why?

→ on small scales in BL,
 ν matters

$$\text{i.e. } Re = Re[\text{scale}]$$

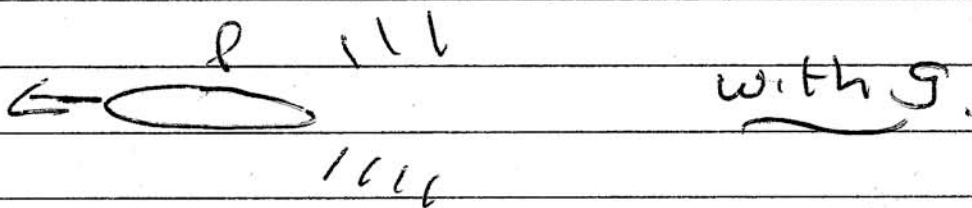
$$= \frac{vL}{\nu}$$

→ but ~~momentum~~ momentum transport
 to small scales independent
 of ν (i.e. inertial).

→ Ex. 2

What are the scaling rules for motion of surface ship of length l , speed V ? Consider:

d.e. Drag scaling? - assume due surface waves
Model size dependence?
streamline

Physics:  with g .

surface ship - modest speed
10-15 m/sec.
- radiates waves.

∞ drag mechanism is radiative
i.e. skin friction - induced stowly down
of chage.

Now, with gravity:

$$\rho_t \underline{V} + \underline{V} \cdot \underline{\nabla} \underline{U} = -\underline{\nabla} \rho - g \underline{\hat{z}} + \nu \nabla^2 \underline{U}$$

Parameters:

$$v \rightarrow L/T$$

$$l \rightarrow L$$

$$\rho_0 \rightarrow M/L^3$$

$$r \rightarrow L^2/T$$

$$F_d \rightarrow M L / T^2$$

and

$$g \rightarrow L/T^2$$

$$\underline{n=6}$$

$$\text{indep: } \underline{n=3} \quad M, L, T$$

$$\Rightarrow \underline{3} \quad \pi \text{ variables}$$

as before:

$$\pi_1 = F_d / \rho_0 l^2 v^2$$

$$\pi_2 = v l / r \equiv Re$$

Need one more dim-less ratio.

now: - obviously must involve g .

- expect $Re \gg \gg 1$.

$$\frac{\textcircled{1}}{\partial_t \underline{V} + \underline{V} \cdot \nabla \underline{V}} = - \frac{\nabla p}{\rho} - g \hat{z} + \nu \nabla^2 \underline{V} \quad \textcircled{2}$$

\Rightarrow

$$\pi_3 \sim \textcircled{1} / \textcircled{2}$$

$$\sim \frac{V^2}{Lg}$$

Froude #
Fr

$$\sim \frac{V^2}{Lg} = Fr$$

\therefore now

$$\pi_1 = \pi_1(\pi_2, \pi_3)$$

\Rightarrow

$$F_d / \rho L^3 V^2 \approx f(Re, Fr)$$

$$\approx f\left(\frac{VL}{\nu}, \frac{V^2}{Lg}\right)$$

Now:

- $Re \rightarrow \infty$, F_d index Re

$$- F_d \approx \rho l^2 v^2 F(v^2/lg)$$

\Rightarrow expect F_d must increase with g

i.e. wave drag increased with g .

v^2 .

$$F_d \approx \rho l^2 v^2 (v^2/lg)^\alpha$$

so $\alpha \approx -1$

$$F_d = \rho l^2 v^2 \left(\frac{lg}{v^2} \right)$$

$$F_d \sim \rho l^3 g$$

For spherical blast, can write eqns of adiabatic gas dynamics as:

$$\partial_t v_r + v_r \partial_r v_r = -\partial_r p / \rho$$

$$\partial_t \rho + \frac{1}{r^2} (r^2 \rho v_r) = 0$$

$$\partial_t (p / \rho^\gamma) + v_r \partial_r (p / \rho^\gamma) = 0$$

seek $\rho(r, t)$, but self-similarity

$$\rho(r, t) = \rho(t) \rho(r / R(t))$$

i.e. solutions look same at different times

\sim blast radius \Rightarrow time prog is re-scaling

\rightarrow spatial structure self-similar, relative to expanding radius.

\rightarrow structure re-scaled on time, preserving shape.

Simple example: wave eqn.

$$\partial_t^2 u = c^2 \partial_x^2 u \quad (\text{1D linear wave})$$

$$u = \frac{1}{2} [F(x-ct) + F(x+ct)] + \frac{1}{2c} \int_{x-ct}^{x+ct} g(\xi) d\xi$$

i.e. $x \pm$ enter as $x \pm ct$ only.

Now, Π -thm. approach: What is radius, in time?

$R \rightarrow$ radius	L
$v \rightarrow$ speed of front	L/T
$\rho \rightarrow$ density	M/L^3
$p \rightarrow$ pressure	$ML^2/T^2 L^3$
$E \rightarrow$ energy	ML^2/T^2

$$\begin{matrix} n = 5 \\ n = 3 \end{matrix} \Rightarrow 2 \text{ } \Pi \text{'s.}$$

$$\Pi_1 = R/vt \rightarrow \text{involved only}$$

$$\Pi_2 = E/\rho R^3 v^2 \rightarrow \text{dimensionless ratio for energy}$$

so

$$\pi_1 = F(\pi_2)$$

i.e.

$$\frac{R}{vt} = f\left(\frac{E}{\rho v^2 R^3}\right)$$

here:

- $f = \text{const} \sim 1$, so

$$R \sim vt$$

- $f = \text{const}$ and/or energy balance

$$E \sim \rho v^2 R^3$$

so

$$v \sim \left[\frac{E}{\rho R^3}\right]^{1/2}$$

and

$$R \sim \left[\frac{E}{\rho R^3}\right]^{1/2} t$$

$$R^{5/2} \sim \left(\frac{E}{\rho}\right)^{1/2} t$$

8

$$R \sim \left(E_0 t^2 / \rho_0 \right)^{1/5}$$

Sedov - Taylor Blast wave radius.

N.B.:

- could just put:

$$E \sim \rho R^3 v^2 \sim \rho R^3 \frac{R}{t^2}$$

$$\rho_0 \sim \rho v^2 \sim \rho_0 R^2 / t^2$$

$$\sim \left(E / \rho_0 \right)^{2/5} \rho_0 t^{-6/5}$$

↓
dynamic pressure drops with time.